

## Diagram to determine pipe dia. and related pressure drop

To get a **rough** idea of the pressure drop sustained in pipes and piping or plumbing units (e.g. elbows, cross-overs, valves, etc.) use the diagram overleaf. This chart is based on 1m length pipes and spec. gravity of 1 kg/dm<sup>3</sup>. For different parameters use the conversion formular.

### 1. Applications

Take the required delivery Q (m<sup>3</sup>/h) and the hypothetical flow rate w (m/s) to determine the pipe dia. d (mm). (Usually between 0.5...0.8 m/s for dosing pumps and 2...4 m/s for constant flow, e.g. for centrifugal pumps).

### 2. Pressure drop through fittings

Determine and **add** the **drag coefficient**  $\xi$  for various controls, elbows, etc. installed in the pipe system. Depending on the previously found/selected flow rate w (m/s) the sum total  $\Sigma\xi$  will give the pressure drop for  $\Delta p_A$  (mbar).

For components built or fitted in the pipe system and not featured in the diagram use  $\xi$ -values.

### 3. Pressure drop through pipes

Determine the pressure drop  $\Delta p_{R1}$  (mbar) per metre piping as a function of the flow rate w (m/s) and the previously established pipe dia. d (mm).

To determine the overall pressure drop  $\Delta p_R$  multiply the value  $\Delta p_{R1}$  by the number of metres of the pipe length.

$$\Delta p_R = \Delta p_{R1} \times \text{pipe length (m)}$$

The pipe was assumed to have a friction or roughness factor of 0.15 mm. This value applies for smooth pipes in process engineering.

### 4. Total pressure drop

The overall accepted pressure drop is the sum total of the pipe and component-governed losses.

$$\Delta p_{\text{total}} = \Delta p_R + \Delta p_A$$

### 5. Specific gravity correction

Pressure drop for liquids with a spec. gravity of  $\neq 1$  kg/dm<sup>3</sup> can be calculated by multiplying the  $\Delta p$ -values found from the diagram by that spec. gravity:

$$\Delta p = \Delta p_{\text{total}} \times \rho$$

### 6. Example

Deliver 0.4 m<sup>3</sup>/h saline solution ( $\rho = 1.18$ ) through the following plant:

Metering pump; 0.5 m PVC tubing; shut-off valve (to DIN); 1m PVC tubing; solenoid valve; flow detector; elbow; flow rate meter; elbow; T piece; 4m PVC-tubing.

Find pipe dia. and pressure drop.

#### Solution:

The pipe diameter is determined to be 16mm at a flow rate of 0.55 m/s.

The sum of the  $\xi$ -values gives us:

DIN standard valve	3.9
Solenoid valve	6.0
Flow detector	5.8
Elbow	0.5
Flow meter	6.5
Elbow	0.5
T Piece	1.3
$\Sigma\xi$	= 24,5




For w 0.55 m/s, and  $\xi=24.5$  the pressure drop in the instrumentation can be found as  $\Delta p_A = 40$  mbar.

Furthermore, at a dia.=16mm, the pressure drop in a 1m long pipe is  $\Delta p_{R1} = 3.5$  mbar.

Thus, the pressure drop to be expected in a 4.5m long pipe system is  $\Delta p_R = 4.5 \times 3.5 = 15.8$  mbar. The overall pressure drop will be the sum total of both these values which has to be multiplied by the  $\rho$ :

$$\Delta p_{\text{total}} = 40 + 15.8 = 55.8 \text{ mbar}$$

$$\Delta p = \Delta p_{\text{total}} \times \rho = 55.8 \times 1.18 = 65.8 \text{ mbar}$$

Inlet/outlet socket (e.g. on the container)		$\xi = 0.06$
		$\xi = 0.56$
		$\xi = 2.8$

Instrument	$\xi$
Ball cock	0.6
Angle seat valve	0.6
Shut-off valve to DIN	3.9
L or T-port valve	3.0
Solenoid valve	6.0
Relief valve	6.0
Flap valve or tapered restrictor	5.8
Floating body/flow-through flow meter	6.5

# Pressure Drops

Elbow		r/d	1	2	4	6	10	
		$\xi$	0.51	0.3	0.23	0.18	0.2	
Bushes/sleeves, restrictors, screwed joints		d/d <sub>1</sub>	0.1	0.3	0.5	0.6	0.8	0.9
		$\xi$	0.45	0.42	0.38	0.3	0.17	0.09
Bend (sharp edge)		$\alpha$	10	15	30	45	60	90
		$\xi$	0.04	0.06	0.15	0.3	0.6	1.2

